

# Mass transfer in a small scale post-combustion flue gas absorber; experiment and modelling

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## Introduction

In this study experimental data of a post-combustion CO<sub>2</sub> capture pilot plant have been compared with a rate-based absorption model. In this model the mass transfer, thermodynamics and kinetics are included. An aqueous solutions of 50 wt.% MDEA has been used to capture the CO<sub>2</sub>.

## Experimental set-up

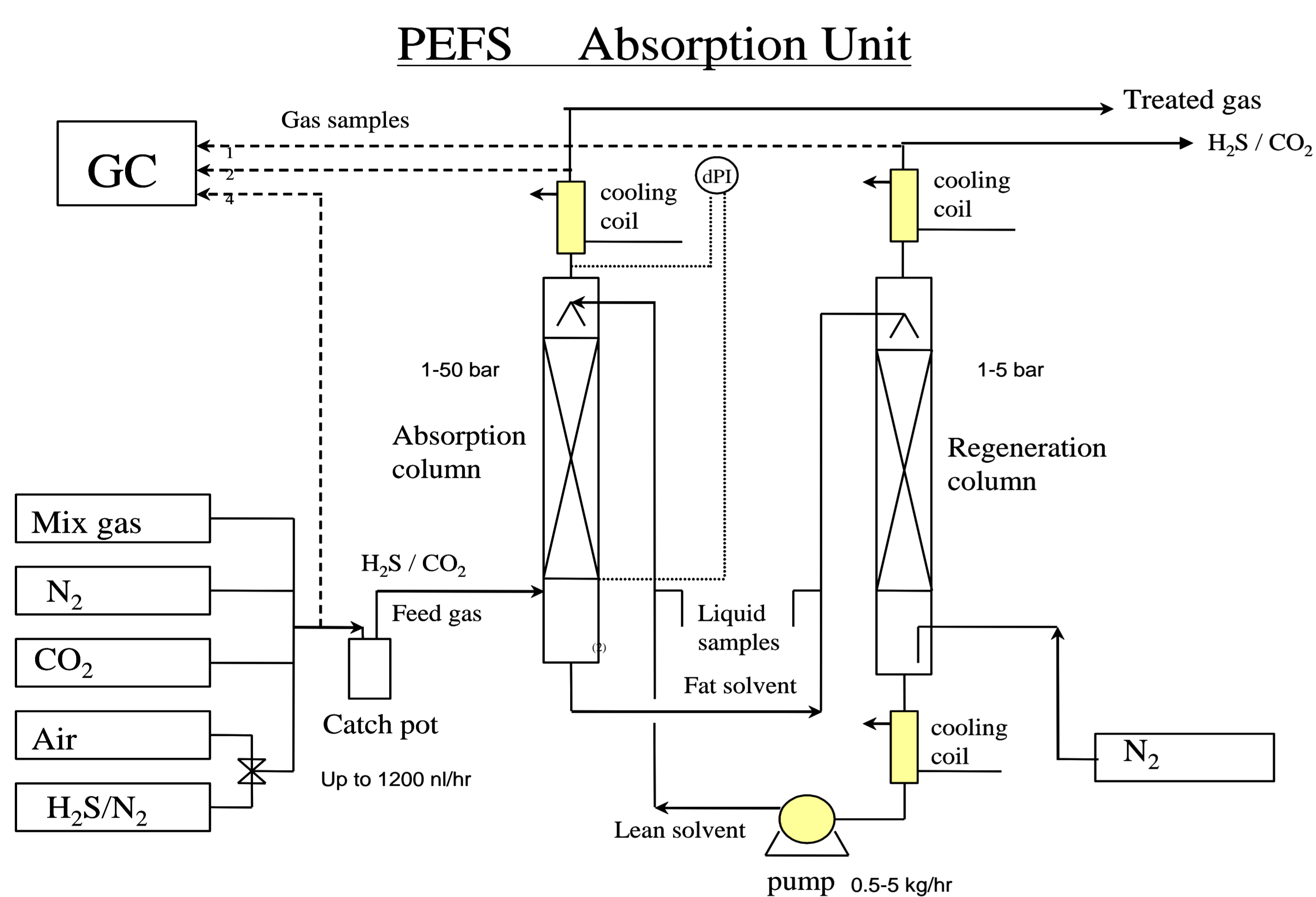


Figure: Flow sheet of the CAPTECH pilot plant unit at Shell Global Solutions

## Absorber:

- Size: D x L = 2.5 x 1450 cm;
- Sulzer EX laboratory packing;
- Aqueous 50 wt.% MDEA;
- Max gas flow: 1.3 Nm<sup>3</sup>.h<sup>-1</sup>;
- Max liquid flow: 6 kg.h<sup>-1</sup>.

## Rate Based Model

Tray to tray procedure for amine blends;

- Mass transfer with complex, reversible chemical reactions;
- Ideal thermodynamic model;
- Mass transfer parameters ( $k_L$ ,  $k_G$  and  $a$ ) from literature correlations;
- Following amines are included: MDEA, DMMEA, DEMA, TEA (tertiary amines) and MEA, DEA, MMEA, DIPA, DGA, AMP (primary / secondary amines).

## Model output:

- Absorber dimensions;
- Temperature profile in the absorber;
- Concentration profile in the absorber;
- Profile of the speciation in the liquid phase.

## Results

Length absorber in pilot plant: 1.45 m;  
Calculated by the rate based model: 1.6 m.

Model not sensitive for  $k_G$ :

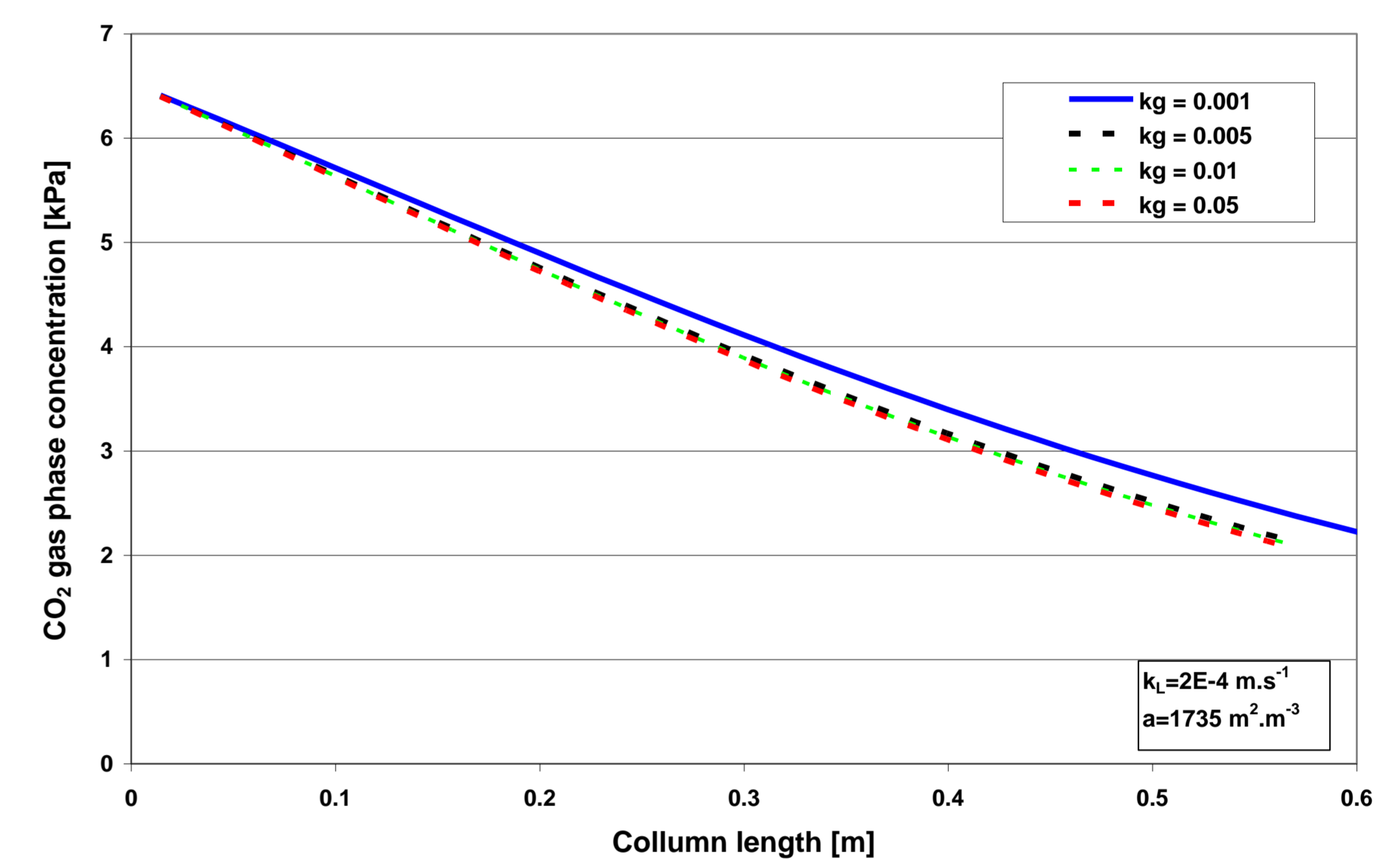


Figure: Influence of  $k_G$  ( $m.s^{-1}$ ) on the calculated absorber dimensions.

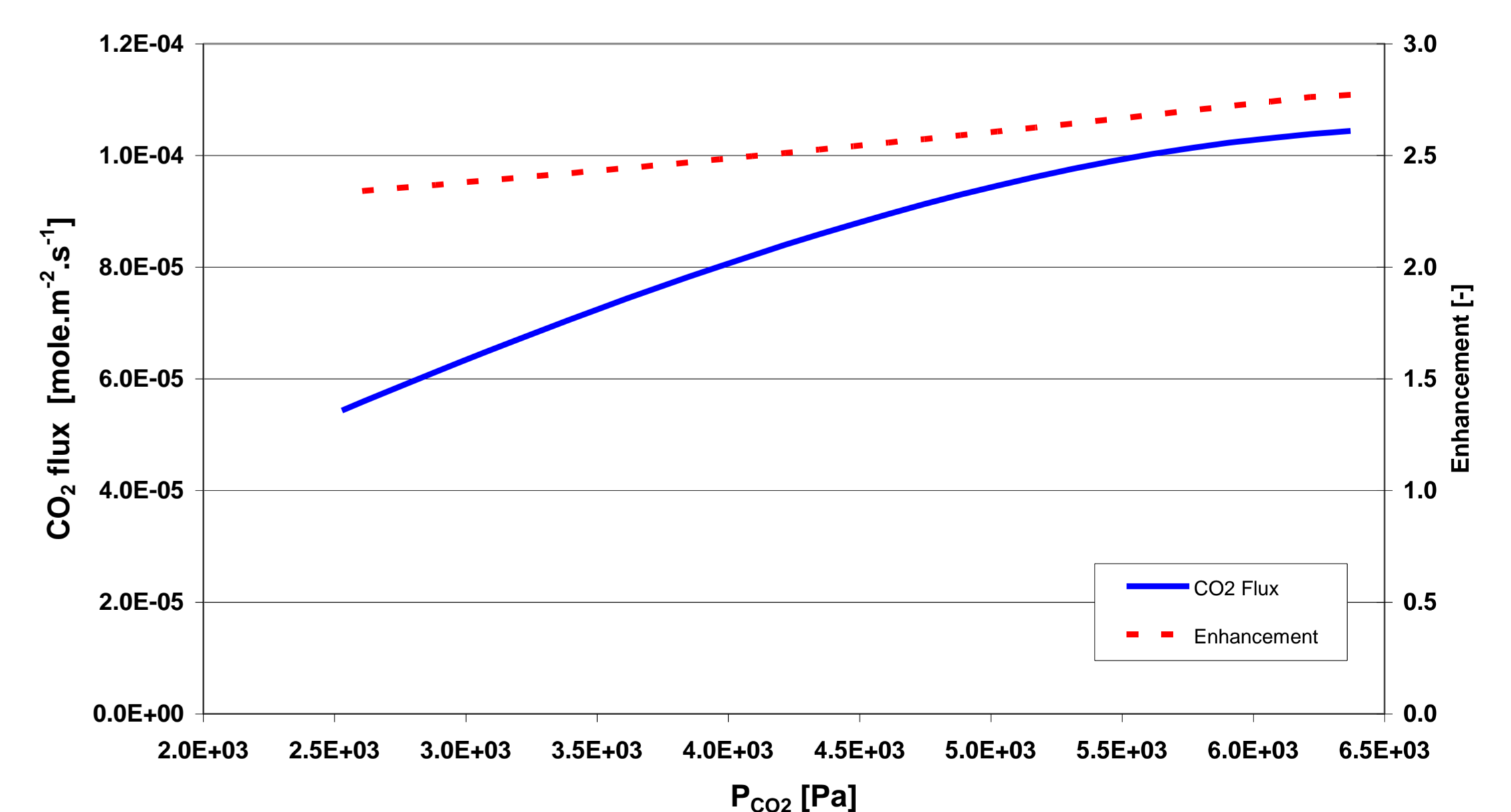


Figure: Calculated CO<sub>2</sub> flux and chemical enhancement in the absorber.

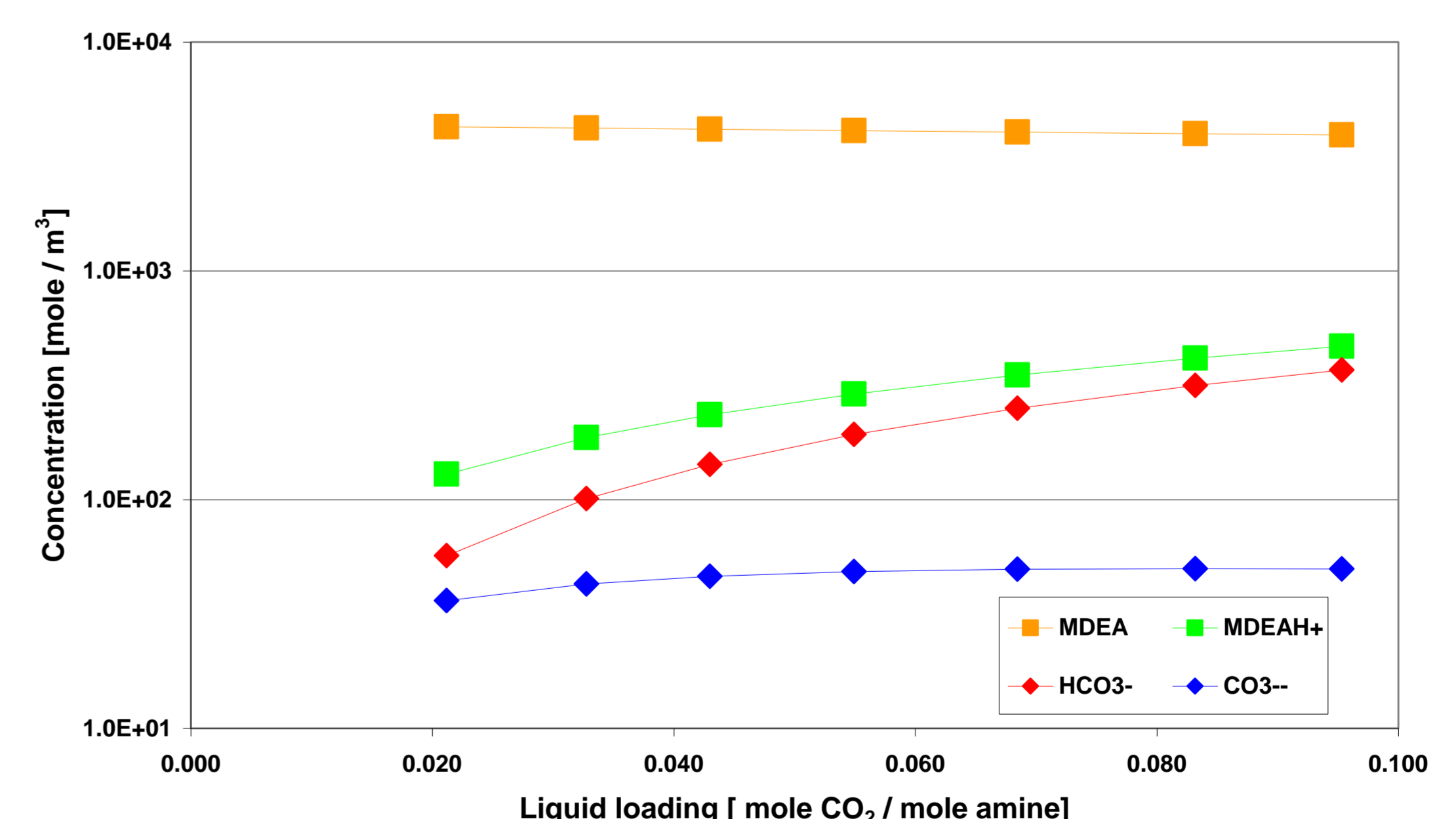


Figure: Calculated liquid speciation in the absorber as function of liquid loading.

## Conclusion

Pilot plant data of a post-combustion CO<sub>2</sub> capture plant have been compared with a rate-based model. With this model it was possible to predict the size of an absorber within an accuracy of 10 %. CO<sub>2</sub> flux, chemical enhancement and liquid speciation were calculated with the model.